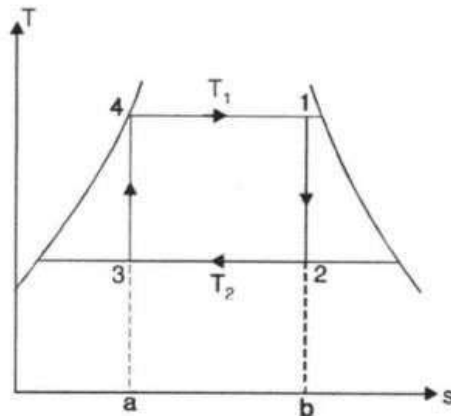


6.8 Solved Numerical

Ex 6.1. [GTU; Jun-2010; 7 Marks]

A Carnot cycle works on steam between the pressures limits of 7 MPa and 7kPa. Determine (a) The thermal efficiency, (b) Turbine work and (c) Compression work per kg of steam.

Solution:



Given Data:

$$p_1 = 7 \text{ MPa} = 70 \text{ bar}$$

$$p_2 = 7 \text{ kPa} = 0.07 \text{ bar}$$

To be Calculated:

a) $\eta_{th} = ?$

b) $w_t = ?$

c) $w_c = ?$

⇒ From Steam Table:

@ $p_1 = 70 \text{ bar}$

$$h_g = 2773.5 \frac{\text{kJ}}{\text{kg}}, s_g = 5.8162 \frac{\text{kJ}}{\text{kg} - \text{K}}, h_f = 1267.42 \frac{\text{kJ}}{\text{kg}}, s_f = 3.1219 \frac{\text{kJ}}{\text{kg} - \text{K}}$$

@ $p_2 = 0.07 \text{ bar}$

$$h_f = 163.38 \frac{\text{kJ}}{\text{kg}}, s_f = 0.5591 \frac{\text{kJ}}{\text{kg} - \text{K}}, h_{fg} = 2409.2 \frac{\text{kJ}}{\text{kg}}, s_{fg} = 7.7176 \frac{\text{kJ}}{\text{kg} - \text{K}}$$

⇒ Enthalpy at point 1,

$$h_1 = (h_{g1})_{@70 \text{ bar}}$$

$$\therefore h_1 = 2773.5 \text{ kJ/kg}$$

⇒ Enthalpy at point 2,

$$h_2 = (h_{f2} + x_2 h_{fg2})_{@0.07 \text{ bar}}$$

But,

$$s_1 = s_2$$

$$(s_{g1})_{@70 \text{ bar}} = (s_{f2} + x_2 s_{fg2})_{@0.07 \text{ bar}}$$

$$5.8162 = 0.5591 + x_2 7.7176$$

$$\therefore x_2 = 0.6811$$

$$\therefore h_2 = 163.38 + 0.6811 \times 2409.2$$

$$\therefore h_2 = 1804.286 \text{ kJ/kg}$$

⇒ Enthalpy at point 3,

$$h_3 = (h_{f3} + x_3 h_{fg3})_{@0.07 \text{ bar}}$$

But,

$$s_3 = s_4$$

$$(s_{f3} + x_3 s_{fg3})_{@0.07 \text{ bar}} = (s_{f4})_{@70 \text{ bar}}$$

$$0.5591 + x_3 7.7176 = 3.1219$$

$$\therefore x_3 = 0.3320$$

$$\therefore h_3 = h_{f3} + x_3 h_{fg3}$$

$$\therefore h_3 = 163.38 + 0.3320 \times 2409.2$$

$$\therefore h_3 = 963.408 \text{ kJ/kg}$$

⇒ Enthalpy at point 4,

$$h_4 = (h_{f4})_{@70 \text{ bar}}$$

$$\therefore h_4 = 1267.42 \text{ kJ/kg}$$

⇒ Heat Supplied,

$$q_s = h_1 - h_4$$

$$\therefore q_s = 2773.5 - 1267.42$$

$$\therefore q_s = 1506.08 \text{ kJ/kg}$$

⇒ The Turbine Work:

$$w_t = h_1 - h_2$$

$$\therefore w_t = 2773.5 - 1804.286$$

$$\therefore w_t = 969.214 \text{ kJ/kg}$$

⇒ The Compression Work:

$$w_c = h_4 - h_3$$

$$\therefore w_c = 1267.42 - 963.408$$

$$\therefore w_c = 304.012 \text{ kJ/kg}$$

⇒ The Thermal Efficiency:

$$\eta = \frac{w_{net}}{q_s} = \frac{w_t - w_c}{q_s}$$

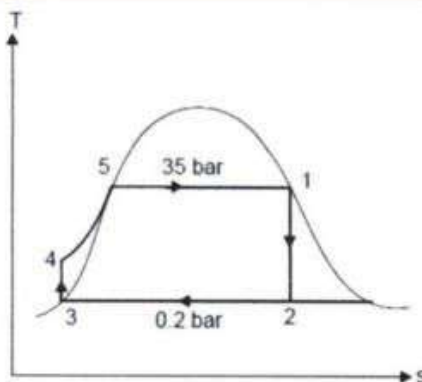
$$\therefore \eta = \frac{969.214 - 304.012}{1506.08}$$

$$\therefore \eta = 0.4416 = 44.16\%$$

Ex 6.2. [GTU; Jan 2015; 7 Marks]

In a Rankine cycle, the steam at inlet to the turbine is saturated at pressure of 35bar and exhaust pressure is 0.2bar. Determine: (a) The pump work, (b) The turbine work, (c) The Rankine efficiency, (d) The quality of steam at the end of expansion. Assume flow rate of 9.5kg/sec. Use of steam table is permitted.

Solution:



Given Data:

$$p_1 = 35 \text{ bar}$$

$$p_2 = 0.2 \text{ bar}$$

$$\dot{m} = 9.5 \text{ kg/sec}$$

To be Calculated:

$$a) w_p = ?$$

$$b) w_t = ?$$

$$c) \eta_{th} = ?$$

$$d) x_2 = ?$$

⇒ From Steam Table:

@ $p_1 = 35 \text{ bar}$

$$h_g = 2802 \frac{\text{kJ}}{\text{kg}}, s_g = 6.1228 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

@ $p_2 = 0.2 \text{ bar}$

$$h_f = 251.45 \frac{\text{kJ}}{\text{kg}}, h_{fg} = 2358.4 \frac{\text{kJ}}{\text{kg}}, s_f = 0.8321 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}, s_{fg} = 7.0773 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

$$v_f = 0.0010172 \text{ m}^3/\text{kg}$$

⇒ Enthalpy at point 1,

$$h_1 = (h_{g1})_{@35 \text{ bar}}$$

$$\therefore h_1 = 2802 \text{ kJ/kg}$$

⇒ Enthalpy at point 2,

$$h_2 = (h_{f2} + x_2 h_{fg2})_{@0.2 \text{ bar}}$$

But,

$$s_1 = s_2$$

$$(s_{g1})_{@35 \text{ bar}} = (s_{f2} + x_2 s_{fg2})_{@0.2 \text{ bar}}$$

$$6.1228 = 0.8321 + x_2 \times 7.0773$$

$$\therefore x_2 = 0.7475$$

$$\therefore h_2 = h_{f2} + x_2 h_{fg2}$$

$$\therefore h_2 = 251.45 + 0.7475 \times 2358.4$$

$$\therefore h_2 = 2014.49 \text{ kJ/kg}$$

⇒ Enthalpy at point 3,

$$h_3 = (h_{f3})_{@0.2 \text{ bar}}$$

$$\therefore h_3 = 251.45 \text{ kJ/kg}$$

⇒ Pump Work,

$$w_p = \int_{P_2}^{P_1} v dP = (v_{f3})_{@0.2 \text{ bar}} (P_1 - P_2)$$

$$\therefore w_p = 0.0010172 \times (35 \times 10^2 - 0.2 \times 10^2)$$

$$\therefore w_p = 3.5398 \text{ kJ/kg}$$

⇒ Pump Power:

$$W_p = \dot{m} \times w_p$$

$$W_p = 9.5 \times 3.5398$$

$$W_p = 33.6281 \text{ kW}$$

⇒ Enthalpy at point 4,

$$w_p = h_4 - h_3$$

$$\therefore h_4 = 3.5398 + 251.45$$

$$\therefore h_4 = 254.9898 \text{ kJ/kg}$$

⇒ Heat Supplied,

$$q_s = h_1 - h_4$$

$$\therefore q_s = 2802 - 254.9898$$

$$\therefore q_s = 2547.01 \text{ kJ/kg}$$

⇒ The Turbine Power:

$$W_t = \dot{m}(h_1 - h_2)$$

$$\therefore W_t = 9.5 \times (2802 - 2014.49)$$

$$\therefore W_t = 7481.345 \text{ kW}$$

⇒ **The Thermal Efficiency:**

$$\eta = \frac{W_{net}}{Q_s} = \frac{W_t - W_p}{\dot{m}(h_1 - h_4)}$$

$$\therefore \eta = \frac{7481.345 - 33.6281}{9.5(2802 - 3.5398)}$$

$$\therefore \eta = 0.2801 = 28.01\%$$

⇒ **The Dryness Fraction:**

$$x_2 = 0.7475$$

6.9 References

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